

# Recovery of Waste Polypropylene & Synthesis of a Sustainable Filament for Additive Manufacturing

## *Group 1:*

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# Overview

- Motivation & Research Objective
- Polypropylene Fundamentals
- STRAP Method
- Additive Manufacturing
- Microcellulose Fundamentals
- Literature Review

# Motivation & Research Objective

Motivation: Covid-19 global pandemic increased plastic pollution

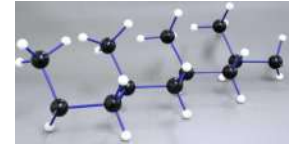
- Estimated global demand of 129 billion face masks per month.<sup>1</sup>
- Additive manufacturing has a need for sustainable materials

Objective: Can we recycle and recover a single-use disposable waste source (i.e., Covid-19 masks) into an extrudable paste for additive manufacturing?

- **Aim 1:** Recover polypropylene (PP) from Covid-19 face mask waste using solvent-recovery techniques
- **Aim 2:** Use the recovered PP to *synthesize* a more sustainable extrudable polymer filament for additive manufacturing
- Use polymer physics fundamentals (i.e., crystalline structure, miscibility, phase separation, cohesive energy density, etc.)



**Aim 1:**  
*Recovery*

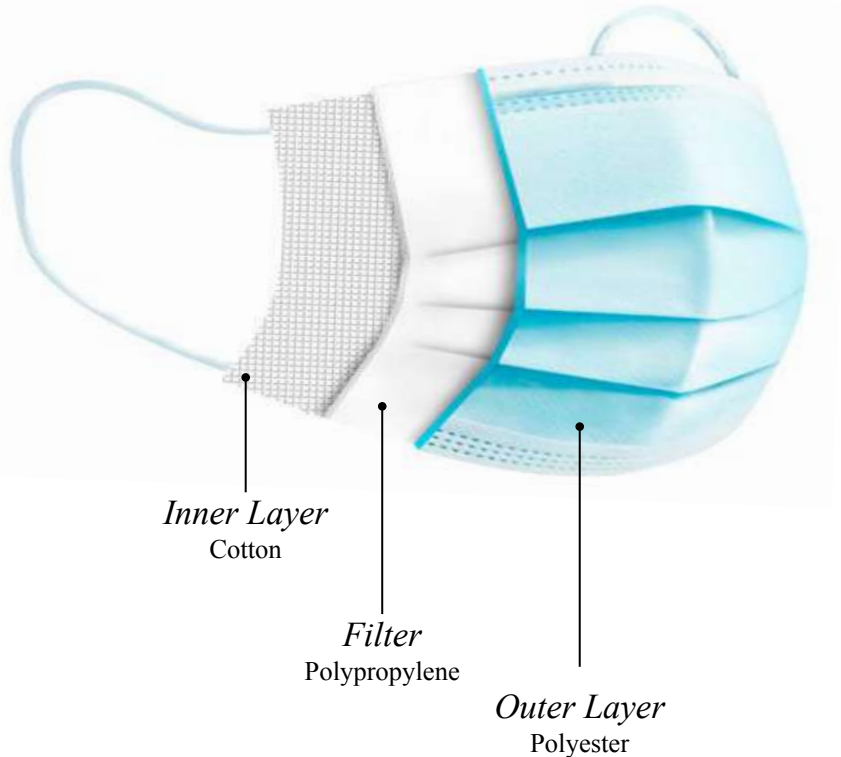


**Aim 2:**  
*Synthesis*



[1] Prata, J. C. *Environ. Sci. Tech.*, vol. 54, no. 13, 2020.

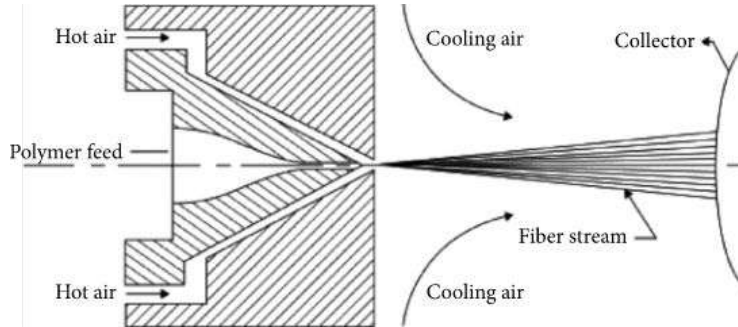
# COVID-19 Face Masks - Material Breakdown



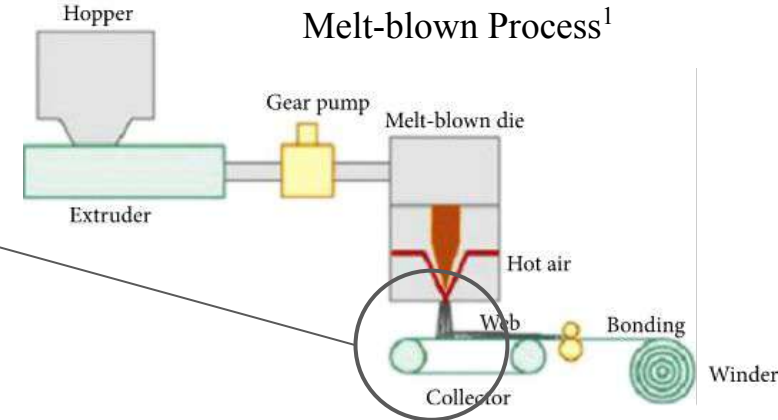
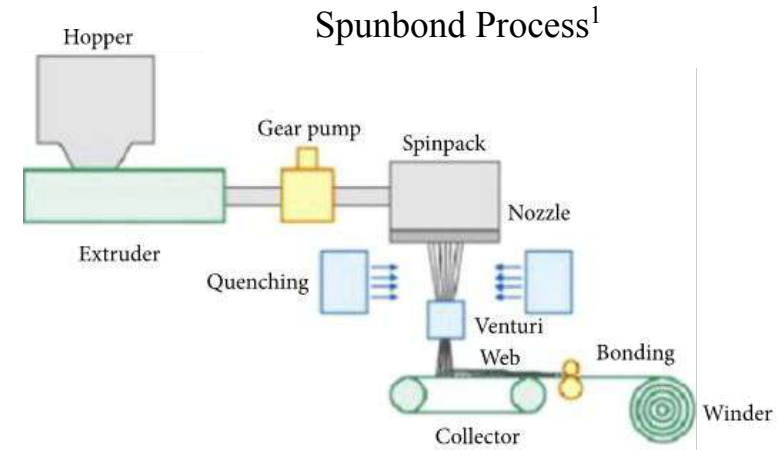
- Mask layers
  - Inner - Cotton
    - Hydrophilic
  - Filter - Polypropylene
    - Hydrophobic
  - Outer - Polyester
    - Hydrophobic
- Recoverable polypropylene (PP)<sup>1</sup>
  - N95 Mask - 11.5 g
  - Blue Disposable Surgical Mask - 4.5 g

# COVID-19 Face Masks - Fabrication

- Nonwovens - fabrics made by entangling fibers
- Nonwoven processes
  - Spunbond
  - Melt-blown



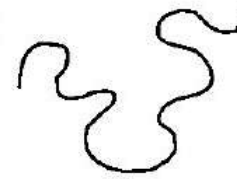
Meltblown Die-Assembly<sup>2</sup>



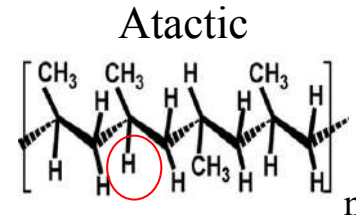
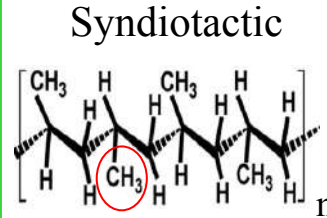
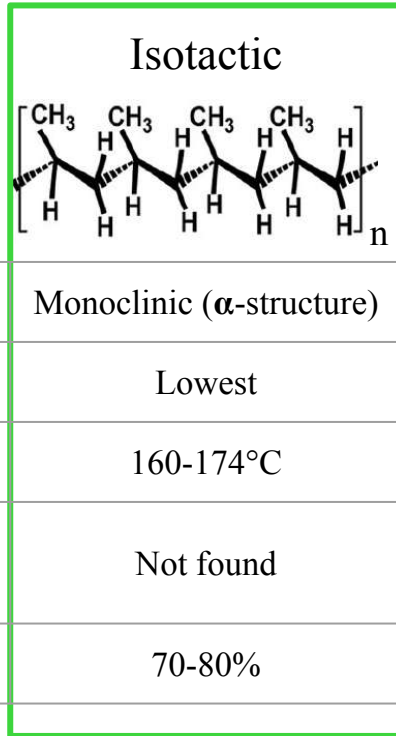
[1] Edwards, et al. *Thomas Net*. (2020).

[2] Hutten. *Handbook of Nonwoven Filter Media*. (2007).

# Polypropylene (PP) Properties <sup>1,2</sup>



Linear architecture of thermoplastics



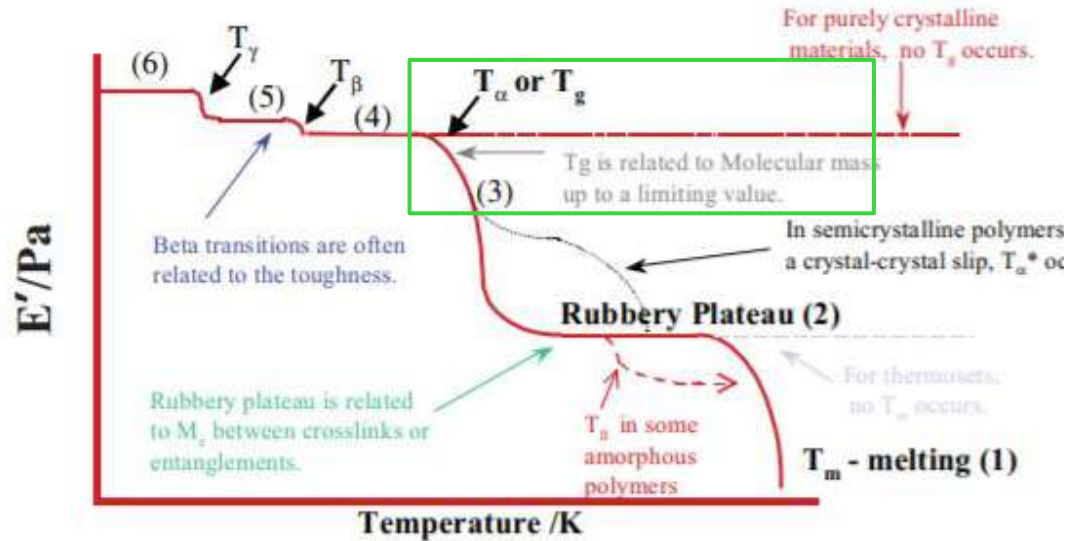
<b>Crystalline Structure</b>	Monoclinic ( $\alpha$ -structure)	Orthorhombic	<b>Crystalline Structure</b>	Not applicable
<b>Free Volume</b>	Lowest	Medium	<b>Free Volume</b>	Highest
<b>Melting Temperature</b>	160-174°C	125-130°C	<b>Melting Temperature</b>	Not applicable
<b>Glass Transition Temperature</b>	Not found	Not found	<b>Glass Transition Temperature</b>	-17 -0 °C
<b>Crystal Ratio</b>	70-80%	~50%	<b>Crystal Ratio</b>	Not applicable

**Isotactic Polypropylene is used in masks**

[1] Hutten. *Handbook of Nonwoven Filter Media*. (2007).

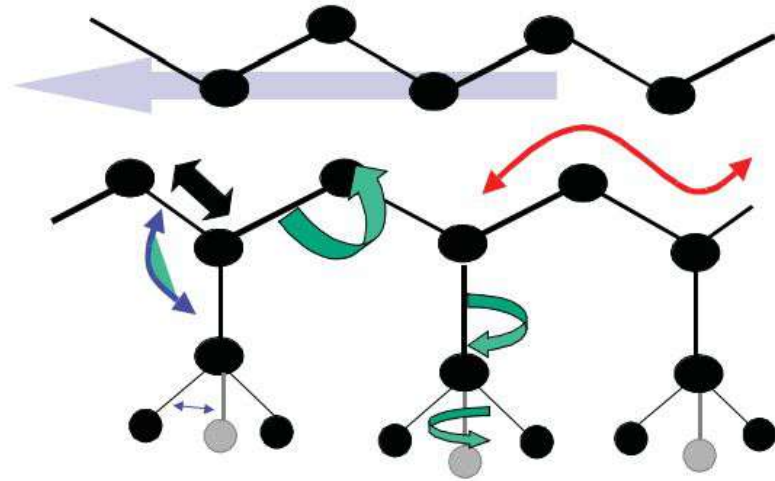
[2] Rubenstein, et al. *Polymer Physics*. (2003).

[3] Natta, et al. "Crystalline Structure of Isotactic Polypropylene." 1967.



- |         |         |        |         |       |          |
|---------|---------|--------|---------|-------|----------|
| (6)     | (5)     | (4)    | (3)     | (2)   | (1)      |
| local   | bend    | side   | gradual | large | chain    |
| motions | and     | groups | main    | scale | slippage |
|         | stretch |        | chain   | chain |          |

## Types of Transitions <sup>1</sup>



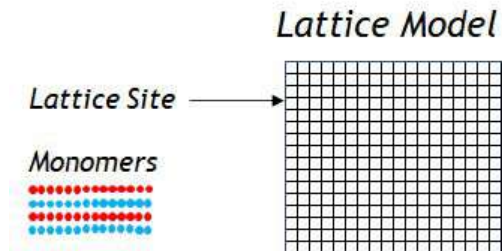
- |                       |         |          |
|-----------------------|---------|----------|
| Stretching            | Bending | Rotating |
| Coordinated movements |         | Slippage |

## Crankshaft Model <sup>1</sup>

[1] PerkinElmer. *Technical Notes: Thermal Analysis*. (2007).

# Flory Mean-Field Theory <sup>1</sup>

- **Model:** Lattice sites
- Lattice sites can be filled with
  - Monomers
  - Solvents
- No double occupancy
- Empty sites are filled
  - **Ignores free volume**
  - Assumes constant volume



# Free Volume (FV) <sup>1</sup>

- Molecules in a liquid ‘occupy’ the majority of a liquid’s volume. The remaining small fraction of the volume that is ‘free’ is used for molecular motion
- Relationships
  - As  $T \uparrow$ ,  $FV \uparrow$
  - As mobility  $\uparrow$ ,  $FV \uparrow$



# Williams, Landel & Ferry (WLF) Equation <sup>1</sup>

- Describes temperature dependence of viscosity on polymer melts

$\eta_0$  = viscosity at reference temperature

B = empirical constant of order unity

f = fractional free volume

$T_\infty$  = Vogel temperature

$$\frac{\eta}{\eta_0} = \exp\left(B \left[\frac{1}{f} - \frac{1}{f_0}\right]\right)$$

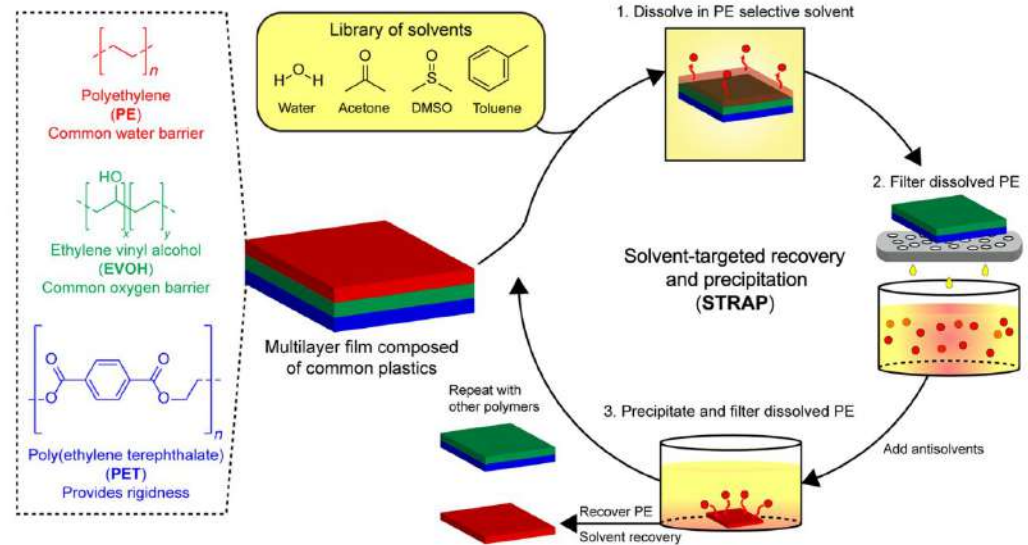
$$\frac{\eta}{\eta_0} = \exp\left(\frac{B}{\alpha_F} \left[\frac{1}{T - T_\infty} - \frac{1}{T_0 - T_\infty}\right]\right)$$

$$\frac{\eta}{\eta_0} = \exp\left(\frac{B}{\alpha_F} \left[\frac{T_0 - T}{(T - T_\infty)(T_0 - T_\infty)}\right]\right)$$

$$\frac{\eta}{\eta_0} = \exp\left(\frac{B}{f_0} \frac{(T_0 - T)}{(T - T_\infty)}\right)$$

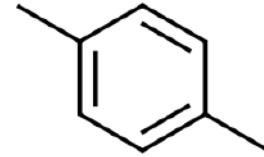
# Solvent-targeted Recovery & Precipitation (STRAP) Method

- Use solvent to selectively dissolve one polymer
  - Only polymer in that layer is soluble in the solvent
- Use filtering & poor solvent to precipitate & recover the soluble polymer
- Use different solvent to target & recover material in next layer
- Utilize Hansen solubility parameters, molecular dynamics, and COSMO-RS

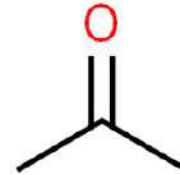


# Solvent Properties

- Good Solvent:
  - Maximize entropy
  - Minimize Gibbs/Helmholtz free energy of mixing
    - **Miscible**
  - PP requires nonpolar solvents such as xylene
- What makes a poor solvent:
  - Positive Gibbs/Helmholtz free energy of mixing
    - **Immiscible**
  - Polymer molecules prefer to interact with themselves than the solvent
  - PP precipitation requires a (polar) poor solvent such as acetone



Xylene (good PP solvent)



Acetone (poor PP solvent)

[1] Rubenstein, et al. *Polymer Physics*. (2003).

[2] Poulakis & Papispyrides. *Resources, Conservation, and Recycling*. (1997).

# Thermodynamics of Mixing

## Entropy

- $S = k \ln \Omega$ 
  - $k =$  Boltzmann constant
  - $\Omega =$  degrees of freedom
- $\Delta \bar{S}_{mix} = -k \left[ \frac{\phi_{PP}}{N_{PP}} \ln \phi_{PP} + \phi_{Solvent} \ln \phi_{Solvent} \right]$ 
  - $\phi =$  volume fraction
  - $N =$  number of occupied lattice sites

## Energy of Mixing

- $\Delta \bar{U}_{mix} = \chi \phi (1 - \phi) kT$ 
  - *Flory Interaction Parameter:*  $\chi \equiv \frac{z}{2} \frac{(2u_{PP\_Solvent} - 2u_{PP\_PP} - u_{solvent\_solvent})}{kT}$

## Helmholtz Free Energy (Flory-Huggins Equation)

- $\Delta \bar{F}_{mix} = kT \left[ \frac{\phi}{N} \ln \phi + (1 - \phi) \ln(1 - \phi) + \chi \phi (1 - \phi) \right]$

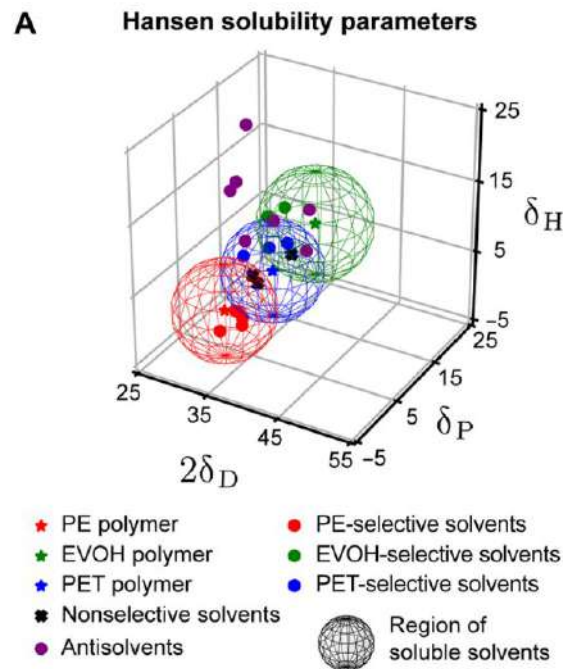
# Solubility Parameters

- Hansen solubility parameters
  - $\delta_D$ : Dispersion (van der Waals)
  - $\delta_P$ : Polarity (related to dipole moment)
  - $\delta_H$ : hydrogen bonding
  - Compares distance between parameters for polymer and solvents (closer distance = better solvent):

$$Ra^2 = 4(\delta D_1 - \delta D_2)^2 - (\delta P_1 - \delta P_2)^2 - (\delta H_1 - \delta H_2)^2$$

- For PP (MPa<sup>1/2</sup>):  $\delta_D = 18.0$ ,  $\delta_P = 0$ ,  $\delta_H = 0$
- Hildebrand/Scott solubility parameter

$$\delta \equiv \sqrt{\frac{\Delta E_{PP}}{V_{PP}}} \quad \rightarrow \quad \chi \approx \frac{v_0}{kT} (\delta_{PP} - \delta_{Solvent})^2$$



[1] <https://www.hansen-solubility.com/HSP-science/basics.php>

[2] Walker et al. Science Advances (Vol. 6, no. 47). 2020.

[3] Rubenstein, et al. *Polymer Physics*. (2003).

# Calculating the Solubility Parameter

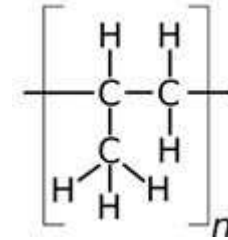
- Solubility can be calculated based on group contributions from functional groups:

$$\delta = \frac{\sum_i F_i^*}{\sum_i V_i^*}$$

- $F_i^*$  = molar attraction constant for  $i$ th group
  - $V_i^*$  = molar volume constant for  $i$ th group
- To calculate the solubility parameter for polypropylene:

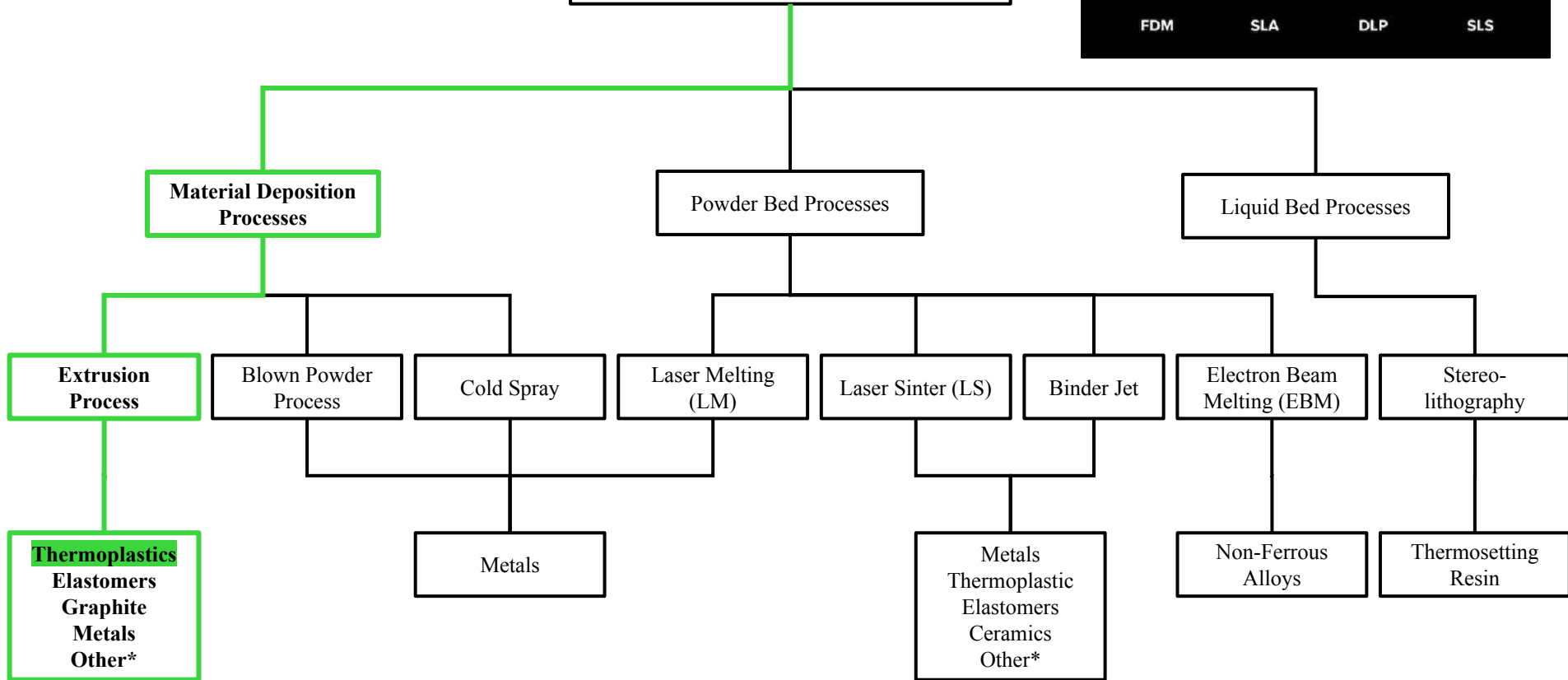
$$(218 + 132 + 23) / (31.8 + 16.5 + 1.9) =$$

$$7.43 \text{ (cal.cm}^{-3}\text{)}^{0.5}$$



Group	Molar Attraction Constant ( $F^*$ , (cal.cm <sup>3</sup> ) <sup>0.5</sup> mole <sup>-1</sup> )	Molar Volume Constant ( $V^*$ , cm <sup>3</sup> mole <sup>-1</sup> )
CH <sub>3</sub>	218	31.8
-CH <sub>2</sub> -	132	16.5
>CH-	23	1.9

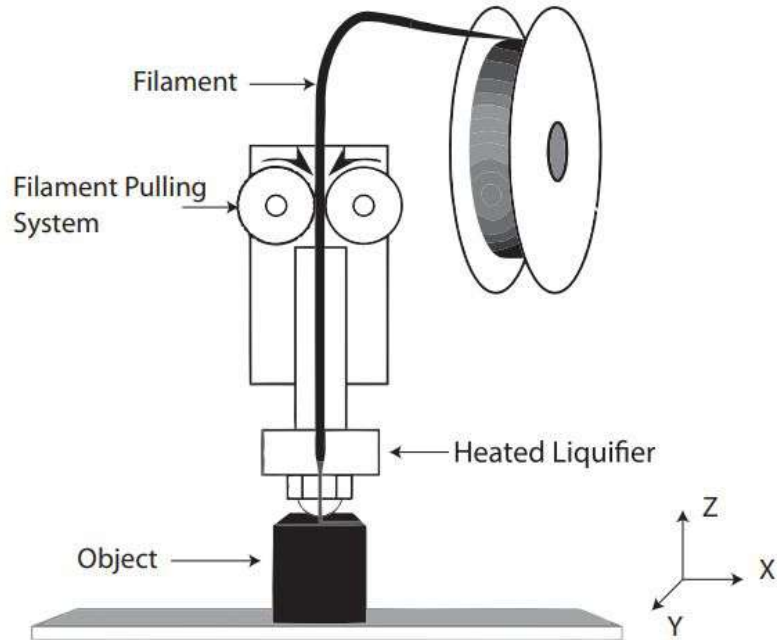
# Additive Manufacturing



\*Can print anything that melts and then hardens

\*Can print anything that is in powder form

# Fused Deposition Modeling (FDM)



Makerbot

- high-quality polymers like ABS, Nylon, Nylon Carbon Fiber, PC-ABS, ASA, PETG, SR-30, PVA, and more.





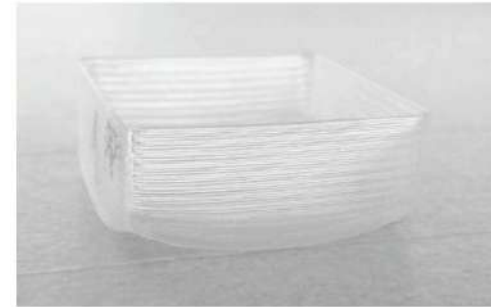
# FDM Printing Challenges with PP

- Larger shrinkage than other polymer filaments (i.e., ABS, PLA, PETG)
  - Crystallization causes decrease in volume
  - Higher shrinkage for lower cooling rates
- Poor bed adhesion
- Lost production time (to deal with issues)
- Thus, PP is not widely used in 3D Printing

Our Solution: include a filler to the PP matrix to modify its physical properties

- Natural fiber filler (green/sustainable material)

Material	Linear Coefficient of Thermal Expansion ( $10^{-5}/^{\circ}\text{C}$ )
ABS <sup>1</sup>	7-15
PLA <sup>1</sup>	8.5
PP <sup>1</sup>	7-17
Cellulose Fiber	1-18

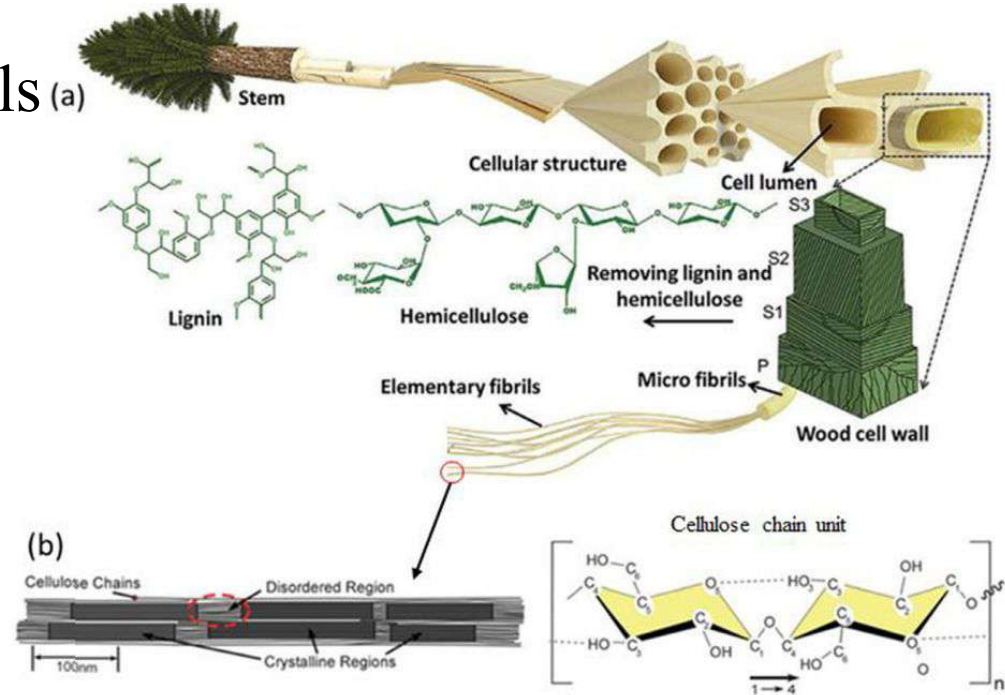


Structure manufactured with fused deposition modeling of polypropylene showing shrinkage after printing.<sup>2</sup>

[1] SpecialChem SA. 2021.

[2] Carneiro, O. S., et al. *Materials & Design*, vol. 83, 2015.

# Microcellulose Fundamentals (a)



## Benefits for thermoplastic polymers

- Highly available (agricultural waste)
- High specific mechanical properties
  - Can be modified by grafting of polymers and other functional groups onto cellulose surface
- **Creates genuine sustainability**

## Uses of cellulose in additive manufacturing:

- Improve interfacial adhesion
- Matrix reinforcement
- Rheology modifier
- Improve thermal stability

## Cellulose fibers are classified by their structure and morphology:

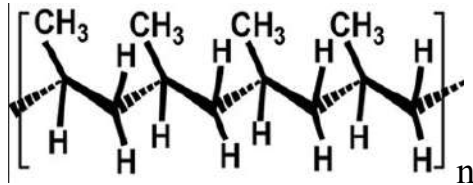
Microcrystalline cellulose (MCC)    Cellulose microfibre (MF):  
 Nanofibrillated cellulose (NFC)    Cellulose nanocrystal (CNC)  
 Bacterial cellulose particles (BC)    Regenerated cellulose (RC)

# Incompatibility of PP + Cellulose Polymer

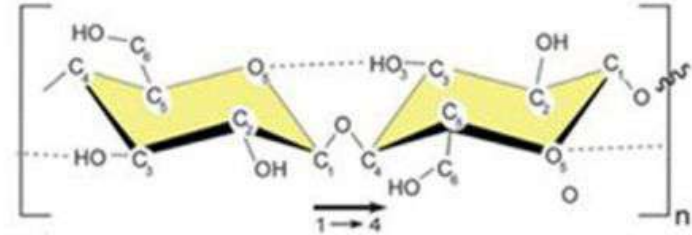
Challenge: *Nonpolar, hydrophobic* PP does not readily mix with *polar, hydrophilic* cellulose fibers (we expect phase separation due to decreased entropy after mixing)

$$\Delta \bar{S}_{mix} = -k \left[ \frac{\varphi_{PP}}{N_{PP}} \ln(\varphi_{PP}) + \frac{\varphi_{cellulose}}{N_{cellulose}} \ln(\varphi_{cellulose}) \right]$$

Isotactic PP



Cellulose chain unit



[1] Rubenstein, et al. *Polymer Physics*. (2003).

[2] Gauss et al. *J. Composites Part C*. (2021).

# Incompatibility of PP + Cellulose Polymer

Hydrophobic-hydrophilic  
Polar-nonpolar

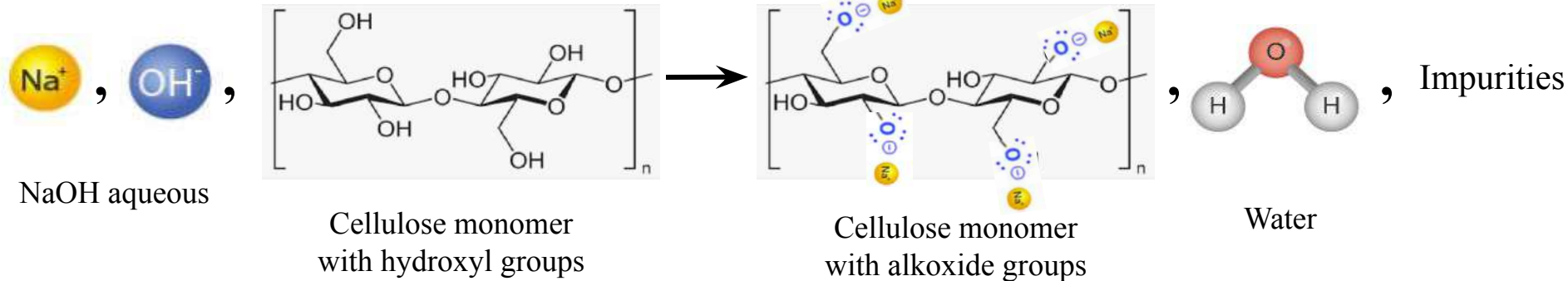
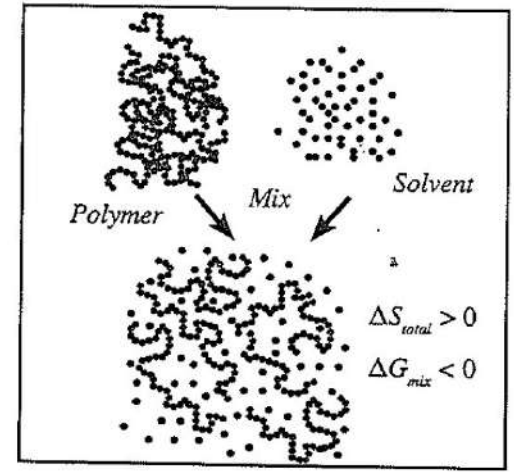
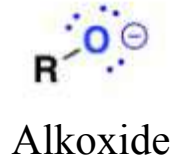
## Solutions:

- 1) *Chemical surface treatment*
  - a) Mercerization (NaOH (aq)) → exposes OH groups on the cellulose surface to increase reactive sites & clean surface
  - b) Esterification → OH groups (hydrophilic) transformed into ester bonds (hydrophobic), improving the natural fiber-PP matrix compatibility
- 2) *Covalently graft* maleic anhydride (MA) to the PP matrix to create maleated PP (MAPP)
  - a) MA group on the MAPP matrix can now react with the OH group on the fiber surface

# (1) Chemical Surface Treatment

## Step a): Alkaline chemical surface treatment

- Cellulose swells in NaOH solvent to expose more reactive sites
- Alkoxide is converted back to OH sites with a water wash
- Purpose: Increases reactive sites (“amorphousness”), cleans surface



# (1) Chemical Surface Treatment

$$\chi = \frac{z\Delta\epsilon_{AB}}{kT}$$

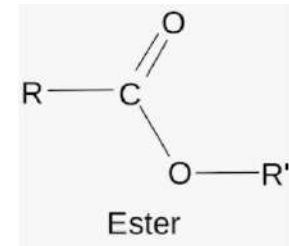
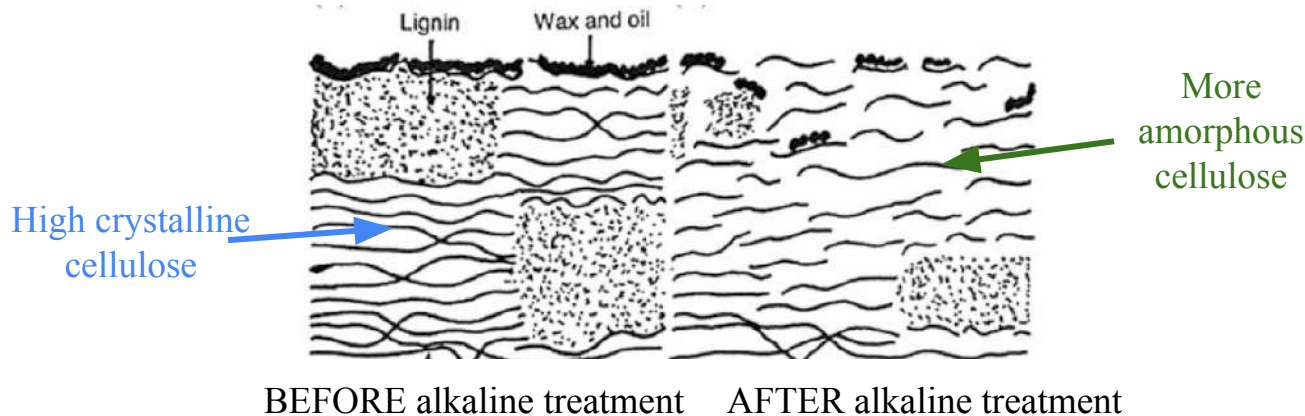
EQUATION 11-25

## Step b): Esterification

$$\frac{\Delta G_m}{RT} = n_A \ln \Phi_A + n_B \ln \Phi_B + n_A \Phi_B \chi$$

EQUATION 11-28

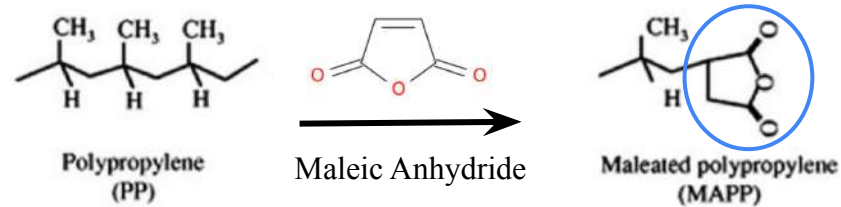
- Cellulose (with lots of OH groups) swells in acetic acid solvent, then reacted with acetic anhydride at high temp.
  - Acetylating agents more likely to react with OH groups in amorphous regions (i.e. lignin, hemicellulose) because *diffusion is difficult in high crystalline regions* (i.e. cellulose)
- Purpose: OH (**hydrophilic**) converted to ester (**more hydrophobic**) so more compatible with PP



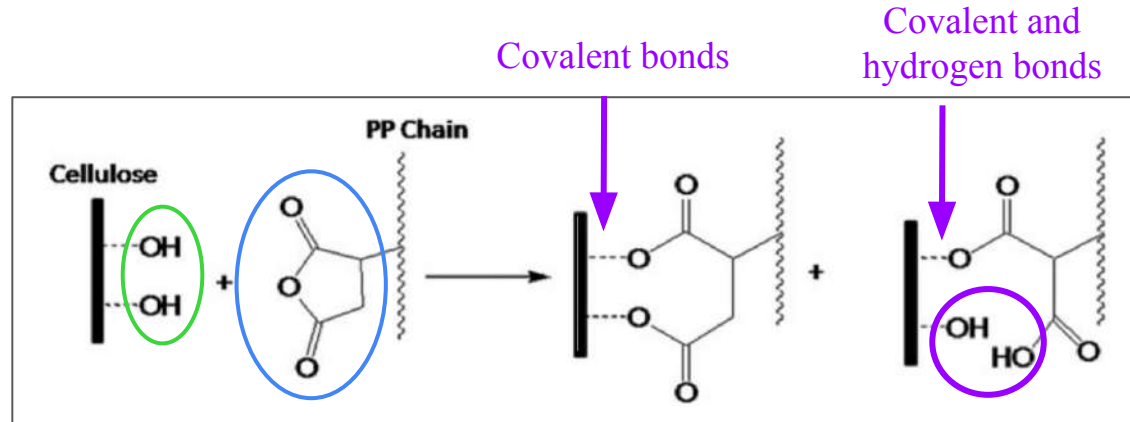
## (2) Covalent Grafting

Polar - Non-Polar

a) *Covalently* graft MA onto PP



b) MA groups on PP will then react with the OH groups on cellulose polymer via *covalent* bonds



- *Surface energy* of cellulose decreases, improving the interfacial adhesion between natural polymer and PP matrix

# Surface Energy - Free Energy of Mixing Relationship

- *Surface energy*  $\Leftrightarrow$  cohesive energy density (CED)  $\Leftrightarrow$  solubility parameter (energy of vaporization)

Hildebrand:

$$\delta_A = C_{AA}^{0.5} \quad \delta_B = C_{BB}^{0.5}$$

EQUATIONS 11-32

$$\Delta H_m = (n_A + n_B)V_m \Phi_A \Phi_B (\delta_A - \delta_B)^2$$

EQUATION 11-33

Flory:

$$\Delta G_m = \Delta H_m - T\Delta S_m$$

Polymer or Blend	Solubility Parameter* (Cal/cm <sup>3</sup> ) <sup>1/2</sup>	CED (Cal/cm <sup>3</sup> )
PP	7.43	55.20
MAPP	9.32	86.86
Cellulose	12.07	145.68
MA-Cellulose	12.30	151.30
Cellulose-MAPP	11.12 (average)	123.65 (average)

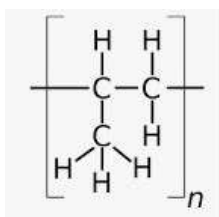
\*calculated using Group Contributions Method



# Solubility Parameter Calculation

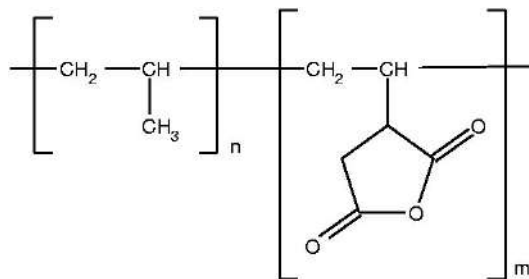
- Group Contribution Method
  - Functional groups influence the energy of vaporization of the overall polymer

## Polypropylene (PP)



$$\delta_{PP} = \frac{218 + 132 + 23}{31.8 + 16.5 + 1.9} = 7.43 \left( \frac{\text{cal.}}{\text{cm}^3} \right)^{0.5}$$

## Maleated Polypropylene (MAPP)



$$\delta_{MAPP} = \frac{218 + 3(132) + 3(23) + 95 + 2(18)}{31.8 + 3(16.5) + 3(1.9) + 5.1 + 2(-2.4)} = 9.32 \left( \frac{\text{cal.}}{\text{cm}^3} \right)^{0.5}$$

$$\delta = \frac{\sum F_i}{\sum V_i} (\text{cal. cm}^{-3})^{0.5}$$

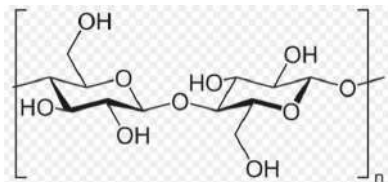
EQUATION 11-38

TABLE 11-1 GROUP CONTRIBUTIONS

GROUP	MOLAR VOLUME CONSTANT $V^*$ ( $\text{cm}^3 \text{ mole}^{-1}$ )	MOLAR ATTRACTION CONSTANT $F^*$ [ $(\text{cal. cm}^3)^{0.5} \text{ mole}^{-1}$ ]
-CH <sub>3</sub>	31.8	218
-CH <sub>2</sub>	16.5	132
>CH-	1.9	23
>C<	-14.8	-97
>C <sub>6</sub> H <sub>5</sub> -	41.4	562
-C <sub>6</sub> H <sub>4</sub> -	58.5	652
C <sub>6</sub> H <sub>5</sub> -	75.5	735
CH <sub>2</sub> =	29.7	203
-CH=	13.7	113
>C=	-2.4	18
-OCO-	19.6	298
-CO-	10.7	262
-O-	5.1	95
-Cl	23.9	264
-CN	23.6	426
-NH <sub>2</sub>	18.6	275
>NH	8.5	143
>N-	-5.0	-3

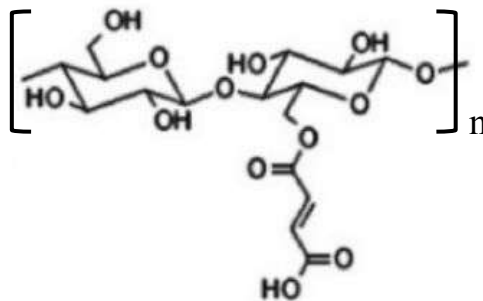
# Solubility Parameter Calculation

Cellulose



$$\delta_{\text{Cellulose}} = \frac{2(132) + 10(23) + 4(95)}{2(16.5) + 10(1.9) + 4(5.1)} = 12.07 \left( \frac{\text{cal.}}{\text{cm}^3} \right)^{0.5}$$

MA-Cellulose



$$\delta_{\text{MA-Cellulose}} = \frac{2(132) + 10(23) + 5(95) + 2(18) + 2(113)}{2(16.5) + 10(1.9) + 5(5.1) - 2(2.4) + 2(13.7)} = 12.30 \left( \frac{\text{cal.}}{\text{cm}^3} \right)^{0.5}$$

$$\delta = \frac{\sum F_i}{\sum V_i} (\text{cal. cm}^{-3})^{0.5}$$

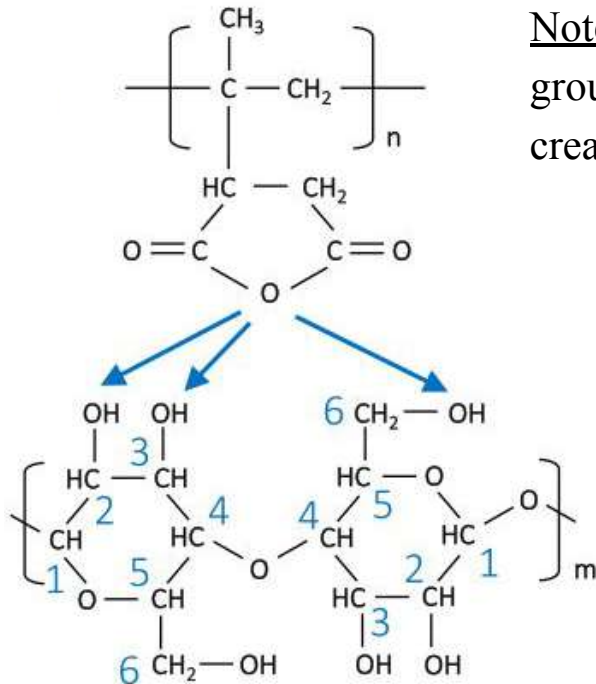
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>CH-	1.9	23
>C<	-14.8	-97
>C <sub>6</sub> H <sub>5</sub> -	41.4	562
-C <sub>6</sub> H <sub>4</sub> -	58.5	652
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CH <sub>2</sub> =	29.7	203
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-OCO-	19.6	298
-CO-	10.7	262
-O-	5.1	95
-Cl	23.9	264
-CN	23.6	426
-NH <sub>2</sub>	18.6	275
>NH	8.5	143
>N-	-5.0	-3

# Cellulose-MAPP Monomer Configurations

## Cellulose-MAPP



Note: MA group can react with cellulose OH groups at the 2, 3, or 6 carbon locations to create...

- Diester bond via covalent bonds
- Monoester bond with covalent and hydrogen bonds (OH group not reacted)
- **Changing the functionals groups will change the solubility parameter!**

$$\delta = \frac{\sum F_i}{\sum V_i} (\text{cal. cm}^{-3})^{0.5}$$

EQUATION 11-38

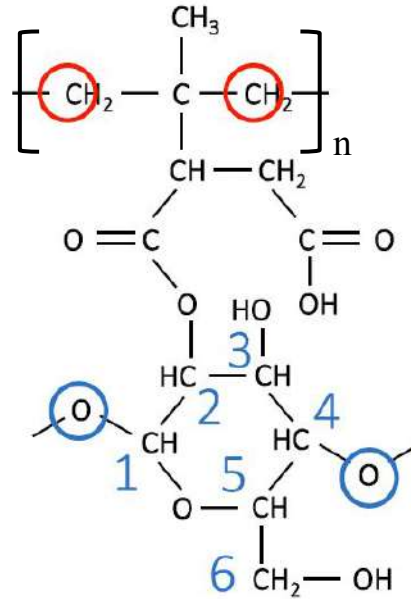
TABLE 11-1 GROUP CONTRIBUTIONS

GROUP	MOLAR VOLUME CONSTANT $V^*$ ( $\text{cm}^3 \text{mole}^{-1}$ )	MOLAR ATTRACTION CONSTANT $F^*$ [ $(\text{cal. cm}^3)^{0.5} \text{mole}^{-1}$ ]
-CH <sub>3</sub>	31.8	218
-CH <sub>2</sub> -	16.5	132
>CH-	1.9	23
>C<	-14.8	-97
>C <sub>6</sub> H <sub>5</sub> -	41.4	562
-C <sub>6</sub> H <sub>4</sub> -	58.5	652
C <sub>6</sub> H <sub>5</sub> -	75.5	735
CH <sub>2</sub> =	29.7	203
-CH=	13.7	113
>C=	-2.4	18
-OCO-	19.6	298
-CO-	10.7	262
-O-	5.1	95
-Cl	23.9	264
-CN	23.6	426
-NH <sub>2</sub>	18.6	275
>NH	8.5	143
>N-	-5.0	-3

# Cellulose-MAPP Monomer: Possibility 1

## Cellulose-MAPP monomer: C2 Model

Possibility 1: MA group reacts with cellulose OH group at the **2 carbon** locations to create a **monoester bond**



$$\delta_{C2 \text{ Model}} = \frac{218 + 4(132) + 6(23) - 97 + 18 + 3(95) + 298}{31.8 + 4(16.5) + 6(1.9) - 14.8 - 2.4 + 3(5.1) + 19.6} = 10.94 \left( \frac{\text{cal.}}{\text{cm}^3} \right)^{0.5}$$

$$\delta = \frac{\sum F_i}{\sum V_i} (\text{cal. cm}^{-3})^{0.5}$$

EQUATION 11-38

TABLE 11-1 GROUP CONTRIBUTIONS

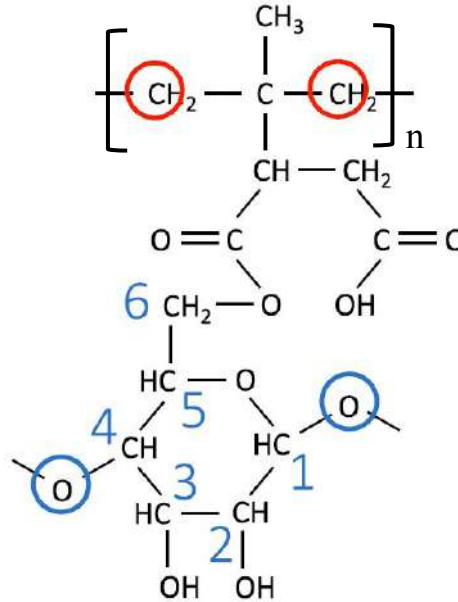
GROUP	MOLAR VOLUME CONSTANT $V^*$ ( $\text{cm}^3 \text{ mole}^{-1}$ )	MOLAR ATTRACTION CONSTANT $F^*$ [ $(\text{cal. cm}^3)^{0.5} \text{ mole}^{-1}$ ]
-CH <sub>3</sub>	31.8	218
-CH <sub>2</sub> -	16.5	132
>CH-	1.9	23
>C<	-14.8	-97
>C <sub>6</sub> H <sub>5</sub> -	41.4	562
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CH <sub>2</sub> =	29.7	203
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-CO-	10.7	262
-O-	5.1	95
-Cl	23.9	264
-CN	23.6	426
-NH <sub>2</sub>	18.6	275
>NH	8.5	143
>N-	-5.0	-3



# Cellulose-MAPP Monomer: Possibility 3

## Cellulose-MAPP monomer: C6 Model

Possibility 3: MA group reacts with cellulose OH group at the **6 carbon** locations to create a **monoester bond**



$$\delta_{C6 Model} = \frac{218 + 4(132) + 6(23) - 97 + 18 + 4(95) + 298}{31.8 + 4(16.5) + 6(1.9) - 14.8 - 2.4 + 4(5.1) + 19.6} = 11.23 \left( \frac{\text{cal.}}{\text{cm}^3} \right)^{0.5}$$

$$\delta = \frac{\sum F_i}{\sum V_i} (\text{cal. cm}^{-3})^{0.5}$$

EQUATION 11-38

TABLE 11-1 GROUP CONTRIBUTIONS

GROUP	MOLAR VOLUME CONSTANT $V^*$ ( $\text{cm}^3 \text{ mole}^{-1}$ )	MOLAR ATTRACTION CONSTANT $F^*$ [ $(\text{cal. cm}^3)^{0.5} \text{ mole}^{-1}$ ]
-CH <sub>3</sub>	31.8	218
-CH <sub>2</sub> -	16.5	132
>CH-	1.9	23
>C<	-14.8	-97
>C <sub>6</sub> H <sub>5</sub> -	41.4	562
-C <sub>6</sub> H <sub>4</sub> -	58.5	652
C <sub>6</sub> H <sub>5</sub> -	75.5	735
CH <sub>2</sub> =	29.7	203
-CH=	13.7	113
>C=	-2.4	18
-OCO-	19.6	298
-CO-	10.7	262
-O-	5.1	95
-Cl	23.9	264
-CN	23.6	426
-NH <sub>2</sub>	18.6	275
>NH	8.5	143
>N-	-5.0	-3

# (Cellulose + MAPP) Polymer Blend Conclusion

**Surface energy** of pure cellulose (proportional to CED = 145.68) **decreases** when cellulose is reacted with the MA group on MAPP (average Cellulose-MAPP CED = 123.65).

- This verifies a statement given by Uetsuji *et al.*

<b>Cellulose-MAPP Blend</b>	<b>Solubility Parameter* (Cal/cm<sup>3</sup>)<sup>1/2</sup></b>	<b>CED (Cal/cm<sup>3</sup>)</b>
C2 Model	10.94	119.68
C2&C3 Model	11.20	125.44
C6 Model	11.23	126.11
<b>Average</b>	<b>11.12</b>	<b>123.65</b>

\*calculated using Group Contributions Method

# (Cellulose + MAPP) Polymer Blend Conclusion

Cellulose + MAPP polymer blend ( $\Delta\delta = 2.75$ ) has the **smallest change in solubility parameter upon mixing** and is therefore, the **most energetically favorable** polymer blend and the **least likely to phase separate**.

$$\Delta\delta_{\text{(Cellulose-MAPP)}} = 2.75 \ll \Delta\delta_{\text{(MACellulose-PP)}} = 4.87$$

corresponding to

$$\Delta G_{\text{(Cellulose-MAPP)}} \ll \Delta G_{\text{(MACellulose-PP)}}$$

Polymer Blend	Change in Solubility Parameter* (Cal/cm <sup>3</sup> ) <sup>1/2</sup>
$\Delta\delta_{\text{(MACellulose-PP)}}$	4.87
$\Delta\delta_{\text{(Cellulose-PP)}}$	4.64
$\Delta\delta_{\text{(MACellulose-MAPP)}}$	2.98
$\Delta\delta_{\text{(Cellulose-MAPP)}}$	2.75

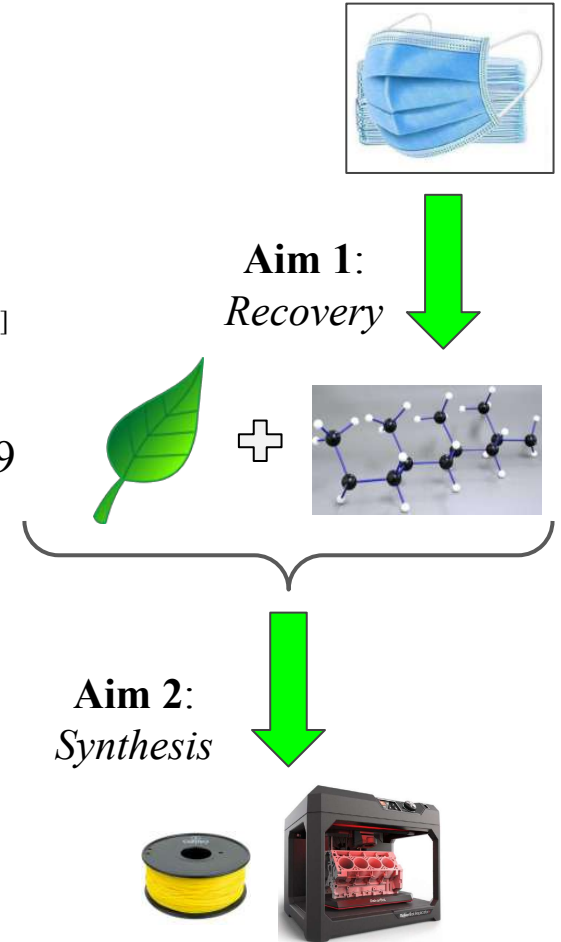
\*calculated using Group Contributions Method

(Cellulose + MAPP) polymer blend is our most stable combination.



# Conclusion

- Motivation: Covid-19 global pandemic increased plastic pollution
  - Estimated global demand of 129 billion face masks per month <sup>[1]</sup>
  - Additive manufacturing has a need for sustainable materials
- Proposal: Recycle & recover a single-use waste (i.e., Covid-19 masks) into an extrudable paste for additive manufacturing
  - **Aim 1**: *Recover* polypropylene (PP)
    - Solvent-Targeted Recovery & Precipitation (i.e., STRAP)
  - **Aim 2**: *Synthesize* a more sustainable extrudable polymer filament
    - Chemical surface treatment of cellulose
    - Covalently graft maleic anhydride (MA) to PP matrix
    - Create miscible cellulose-MAPP blend



# Thank You!

Are there any questions?

